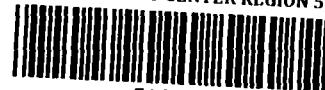


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US EPA RECORDS CENTER REGION 5



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C O P Y

Carl
REILLY TAR & CHEMICAL CORPORATION

DR. W. R. WHEELER - INDPLS.

St. Louis Park

MR. H. L. Finch

March 2, 1970

AIR POLLUTION - ST. LOUIS PARK

Considerable time has passed since your letter of December 8, 1969 but really the urgency has not been postponed. In the third paragraph of your letter you ask if I feel the total air gas of 400 SCFM would be adequate. With the fan that we do have we are not experiencing any difficulty in venting the pans. We have had difficulty with the accumulation of naphthalene at the fan after passing through the scrubber.

We have constructed a cooler to remove more oil and solids and will install this prior to the scrubber.

The 4" pitch line running to the boiler is now used to transfer creosote oil from the refinery to the treating plant and, therefore, could not be tied up to route the air gas mixture to the boilers. I do like the idea, however, of routing our air gas mixture from the refinery to the boiler operation for burning. By routing the air gas mixture to the boilers we are utilizing the heat necessary to promote combustion of the air gas mixture and, of course, we will receive the benefits of any heat as a result of the combustion. Should a portion of the air gas mixture not burn in the boiler operation we have the benefit of a high smoke stack to dissipate any carry over. As I understand your alternative suggestion, the burning would be done in a near proximity of the refinery with the flow being continuous while firing the stills. I am somewhat leery about the flare type burning device. I am taking the liberty of discussing our problem more in detail with the Minneapolis Gas Company and will follow up with you on this discussion.

The treating cylinder ejector is a #10 AL Ellicott Steam Jet ejector SN 27357 with a drawing reference of Z 80079 shows 750 lbs. of dry air per hour at 6°, 2,350 lbs. of steam per hour.

The water is available through the city water system which would be costly. The drain would be now to our open ditch system. It might well be that we would have to plan to run this water through a possible proposed separator for handling all our process water before going into a sanitary sewer.

The idea of a cooling tower has greater appeal to me now as I do not wish to compound a drainage problem that I already have.

Mr. Justin has been investigating the control of the water temperature in our distillate condensers coming from the stills. It has been found that by keeping the water in our distillate condensers circulating more rapidly a noticeable reduction in the odors coming from the vent pan resulted. The cooling pond that we have is not of

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Dr. W. R. Wheeler - Indpls. (Page 2)

sufficient size so that we can circulate the water from the pond through the condensors and back to the pond and have a good control of the temperature of the water in our condensers. We have been recently pumping direct from our well through the condensers and back to our pond.

It would appear that a control of the temperature of the cooling water around our distillate tubes passing through the condenser should be instituted. We, of course, have a problem of water disposal but with the possibility of going into a storm sewer, this water should be no problem in the future. Since this water is obtained from our own well system, the cost of the water would be the operation of the pump. The well from which we obtain this water is in the neighborhood of 650 feet deep.

This well is not all roses, however, since we have had problems in the past of bringing a tar substance to the surface in small balls which has a tendency to stick our pump from time to time. At one time we were going to install a pressure system using this well to supply the water. To get a sufficient supply of water from this well to use in our pressure system, we brought up a considerable amount of sand and the small tar balls, causing the idea to be abandoned. It might well be that we could throttle down the pump and not draw as much water from the well as we had intended to draw under a pressure system and get a sufficient supply of continuous water at reduced gallons per minute and not encounter the problem heretofore mentioned.

Yours very truly,

H. L. Finch

HLF:ge

cc: Mr. T. J. Ryan - Indpls.
Mr. R. J. Hennessey - Reilly Lab.
Mr. H. R. Horner - Reilly Lab.

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Mr. R. H. Hartman
Mr. F. J. Moore
Mr. T. E. Hartman
Hartman

H. C. P. 100

RECEIVED
H. C. P. 100

RECORDED IN THE OFFICE OF THE SECRETARY OF STATE FOR THE STATE OF CALIFORNIA
ON THIS DAY OF SEPTEMBER TWENTY EIGHT, IN THE YEAR OF NINETEEN HUNDRED EIGHTY EIGHT.
IN WITNESS WHEREOF, I have signed my name to this instrument.

I, JOHN HARTMAN, do not believe that either of the two above mentioned
had a discussion with me relating to the proposed transaction, nor
was there any communication between us concerning the same.

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had a discussion with me relating to the proposed transaction, nor
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had a discussion with me relating to the proposed transaction, nor
was there any communication between us concerning the same.

JOHN HARTMAN - H. C. P. 100

SEPTEMBER 31, 1960

H. C. P. 100

REPUBLIC CRESOTING COMPANY

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